# An Interactive Software Tool for the Study of Event-based PI Controller

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**Abstract:** The paper describes an interactive tool focused on the study of a new family of event-based PI controller. Most research in control engineering considers periodic or time-driven control systems. Event-based control is particularly a very promising alternative when systems with reduced computation and communication capacities are considered. For event-driven controllers it is the occurrence of an event, instead of the autonomous progression of the time what decides when the signal sampling should be made. The tool has been developed using Sysquake, a Matlab-like language with fast execution and excellent facilities for interactive graphics. The highly visual and strongly coupled nature of event based control system is very amenable to interactive tools. The tool presented in this paper enables to discover a myriad of important properties of these systems.

# 1. INTRODUCTION

Research carried out in automatic control considers in most cases periodic control systems where continuous-time signals are represented by values sampled with a sampling period h. These systems are designated generically as time-based control systems. On the contrary in an event-based control system is the occurrence of an event, rather than the passage of time, what decides when to sample the dynamic system. This means that in a time-based control system is the autonomous progression of the time what triggers the execution of actions while in an event-based control systems is the dynamic evolution of the system that decides when the next control action will be applied.

The fundamental reason for the predominance of time-based control systems has been based on the existence of a theory well established and mature for sampled data control systems (Åström and Wittenmark, 1997). There are many practical situations where it is interesting and advantageous to consider event-based control systems instead of the traditional time-based control system. Mechanism of activation by events can vary depending on the case (Årzén, 1999). Some significant examples are (Åström, 2007 and Heemels et al., 2008):

Control of internal combustion engines is an example where variable sampling intervals appears in a natural way because it is sampled with respect to the speed of the machine. The nature of the event-based sampling can be intrinsic to the method of measurement used or physical nature of the process that is being controlled. For example, when using encoders sensors to measure the angular position of a motor. Control systems that incorporate relays are another example that can be considered as a special case of event-based sampling. Event-based sampling can also be a built-in feature incorporated into a smart sensor device. In many cases it is natural for example when used as sensors encoder or when the actuators are of on-off type nature, such as in satellite thrusters, or in pulse–width of pulse frequency modulation.

Event-based sampling is also used in the process industry when using closed-loop control of statistical process (SPC) concept. To avoid disturbing the process, a new control action is calculated only if there is a statistically significant deviation. Another case of this kind is a manufacturing system where the sampling is related to the rate of production. Modulators  $\Delta$ - $\Sigma$  or the one-bit A/D converters normally used in mobile phones are also special cases of event-based control.

In addition to different natural sources of triggering events and their relevance in practice, there are many other reasons why the use of an event-based control is of interest.

Event-based control is much closer to the way in which human beings act as a controller. In reality, when an operator realizes manual control his behaviour is guided by events rather than by time. No control action is taken until the measurement signal has diverged enough from the set point.

Another important reason for the interest of event-based control comes from the hand of the use of the computing resources. An embedded controller is typically implemented in a real time operating system. The available CPU time is shared between the tasks in a manner such that it seems that each one runs independently. Having occupied the CPU doing control calculations when nothing significant has happened in the process is clearly an unnecessary use of available resources.

The same argument also applies to communication systems. The communication bandwidth that is available in a distributed system is limited. Use it to send data through a time-based control scheme implies a loss of bandwidth. If the number of updates of the control signal sent across the network is reduced, the bandwidth will be increased. This means a reduction in the number of messages that is transmitted directly and thus produces a decreasing in the average bus load.

Another example is a wireless sensors network, where each sensor node is powered by a battery. The experiences carried out by (Feency and Nilsson 2001) show that comparatively wireless transmissions consume relatively more energy than required for the own internal calculations and it is therefore a limiting factor of their autonomy. Therefore to reduce consumption energy, it would be desirable an event-based sampling method requiring less data transmissions.

The event-based control considered in this paper is a new event-based PI controller where a two-degree-of-freedom (2DOF) structure is used to cope with the set-point following and the load disturbance rejection tasks (Sánchez et al., 2011). As in other event-based controllers, a deadband around the set-point value is considered. Then an event-based feedforward controller allows a transition of the process output to a new reference value  $y_{sp}$  by just two control actions: the two events that trigger the controller and the two corresponding control actions are pre-calculated by a design method that requires a first-order-plus-dead-time (FOPDT) model. Once the process is inside the deadband, an eventbased feedback PI controller is in charge of rejecting disturbances and maintaining the process inside the band. The coupling of the feedforward and feedback parts is based on an estimate of the error area to detect the presence of disturbances or on a variable dead band derived from the FOPTD model.

The motivation of the 2DOF event-based proposal is twofold: first, to present an event-based counterpart for the wellknown 2DOF PI controller by exploring new event-based designs, and second, to improve the set-point following task from an event-based point of view. Like any time-based feedforward design, the event-based alternative improves the process response, but it also offers another improvement: a significant reduction in the number of events during the setpoint task (just two control actions) without a significant worsening of the response (one of the key issues of any event-based control design). This issue has not been addressed in previous works on event-based PI control.

Automatic control ideas, concepts and methods are really rich in visual contents that can be represented intuitively and geometrically. These visual contents can be used for presenting tasks and handling concepts and methods, and manipulated for solving problems. The basic ideas of automatic control often arise from very specific and visual situations. All experts know how useful it is to go to this specific origin when they want to skilfully handle the corresponding abstract objects. The same occurs with other apparently more abstract parts of automatic control. Using visual images and intuition, control specialists are able to relate constellations of facts that are frequently highly complex and the results of their theories in an extremely versatile and varied way. Our feeling is primarily visual and it is thus not surprising that visual support is so present in our work. Control experts very often make use of visual diagrams and other forms of imaginative processes in their work and they acquire what could be called an intuition of what is abstract. Visualization thus appears to be something natural both in the origins of automatic control and the discovery of new relations between mathematical objects.

Traditionally, the design of the systems is carried out following an iterative process. Specifications of the problem are not normally used to calculate the value of the system parameters because there is not an explicit formula that relates them directly. This is the reason to split each iteration in two phases. The first one, often called synthesis, consists of calculating the unknown parameters of the system taking as a basis a group of design variables (that are related to the specifications). During the second phase, called analysis, the performance of the system is evaluated and compared to the specifications. If they do not agree, the design variables are modified and a new iteration is performed. It is possible; however, to merge both phases into one and the resulting modification in the parameters produces an immediate effect. In this way, the design procedure becomes really dynamic and the users perceive the gradient of change in the performance criteria. This interactive capacity allows us to identify much more easily the compromises that can be achieved in a control design problem.

In control education many tools have been developed over the years with these aims. Many interesting ideas and concepts were implemented by Prof. Åström and col. at Lund. In this context we should highlight the concepts of dynamic pictures and virtual interactive systems introduced by Wittenmark (Wittenmark et al., 1998). In essence, a dynamic picture is a collection of graphical windows that are manipulated by just using the mouse. If we change any active element in the graphical windows an immediate recalculation and presentation automatically begins. Thus we can perceive in an immediate and coherent way how their modifications affect the result obtained. The interactive tool that we present in this paper is coded in Sysquake, a Matlab-like language with fast execution and excellent facilities for interactive graphics, and is delivered as a stand-alone executable that makes it readily accessible to users (Piguet, 2004).

The paper is organized as follows. In Section 2 the basic properties of the two-degree-of-freedom PI controller based on events are summarized. The results are based on (Sánchez *et al.*, 2011) where many additional details are given. A summary of the tool's functionality is presented in Section 3. Finally, Section 4 presents the main conclusions.

# 2. STRUCTURE OF THE 2DOF PI CONTROLLER

The block diagram of the 2DOF event-based controller is shown in Figure 1. For the sake of clarity, the event detection logic of both controllers is located inside one block. The purpose of this logic is similar to the clock in the computer implementation of time-driven controllers, i.e., to determine the generation of a new control action. In this case, the generation of the control actions  $u_{ff}$  and  $u_{fb}$  by the compensators  $C_{ff}$  and  $C_{fb}$  is triggered by state events obtained from the set-point value and the control error signal.

The rationale of the event-based feedforward compensator  $C_{ff}$ is as follows. First, an open-loop control action is designed to move the process towards the reference  $y_{sp}$ , and second, a two-event-based proportional controller that produces a control action similar to the feedforward one is calculated off-line (Visioli, 2004). The Cff controller is in "closed-loop" under just two conditions: when a new reference value is introduced and when the process output is crossing a certain threshold value  $y_{\tau}$ . Based on it, and on a FOPDT approximation of the original process, a generic tuning formula to obtain  $K_p^{ff}$  and  $y_{\tau}$  is derived. Once the process reaches  $y_{sp}$  thanks to  $C_{ff}$ , the event-based controller  $C_{fb}$  is enabled to cope with disturbances  $C_{fb}$  starts calculating proportional and integral actions only when the process output moves outside the dead band, and it stops when the process output is again inside the band.

### 2.1 The event-based feedforward controller $C_{\rm ff}$

We assume that the process to be controlled has FOPDT dynamics, namely:

$$P(s) = \frac{K}{Ts+I}e^{-Ls} \ . \tag{1}$$

Then, without loss of generality, we assume that, starting from null initial conditions, a process output transition from 0 to  $y_{sp}$  is required.



Fig. 1. Block diagram of the 2DOF event-based PI controller

Figure 2 shows the open-loop situation to be repeated by  $C_{ff}$  and the two events where the control action must change. The set-point following task when a new set-point value  $y_{sp}$  is applied to the control system is given by the following algorithm:

1. Determine the parameters *K*, *T*, and *L* of the model (any procedure for this purpose can be applied (Visioli, 2006)).

2. Determine the proportional gain  $K_p^{ff}$  from:  $(1 - e^{L/T})X^2 - (1 - e^{L/T})X + 1 = 0$  where  $X := KK_p^{ff}$ 



Fig. 2. Open-loop process response to be repeated in closed loop by the two-event-based controller  $C_{ff}$ .

3. Determine the value of  $y_{\tau}$  using:

$$\tau = -T \log \left( 1 - \left( KK_p^{\text{ff}} \right)^{-1} \right) \text{ and } y_\tau = KK_p^{\text{ff}} y_{sp} \left( 1 - e^{-((\tau - L)/T)} \right)$$
  
4. Define  $e_\tau := y_{sp} - y_\tau$ .  
5. If  $\left( |e(t)| > |e_\tau| \right)$  then apply  $u_{\text{ff}}^1 = K_p^{\text{ff}} y_{sp}$   
6. If  $\left( |e(t)| \le |e_\tau| \right)$  then apply  $u_{\text{ff}}^2 = K_p^{\text{ff}} \left( y_{sp} - y_\tau \right)$ 

It is important to note that, in the absence of load disturbances and model mismatches during the transition from 0 to  $y_{sp}$ , the process output will reach the  $y_{sp}$  value after just two control actions.

### 2.2 The event-based feedback controller $C_{fb}$

To offer a complete controller, the disturbance rejection task must be addressed as in any other controller, but this time with an event-based solution. As was said, from the first time that the process enters the dead band, a feedback controller  $C_{ff}$  will be in charge of compensating for any disturbance. This controller is a PI controller where the activation of the proportional and integral parts is triggered by two types of asynchronous events. The P and I parts are enabled once the process is inside the dead band, and they start calculating at the very moment that the process leaves the band as the result of a disturbance. The event-based solution consists of applying a level crossing sampling strategy to each part to trigger the computation of the control action. Briefly, to sample a signal x(t) by level crossing means to take a new sample every time that the difference in the signal with respect to the last sample is higher than a certain threshold value  $\delta$ . It can be expressed by the following logical expression:

$$|x(t) - x(t_1)| \ge \delta \tag{2}$$

where x(t) is the current value of the signal and  $x(t_1)$  is the value of the signal the last time the logical condition was true. The level crossing is the simplest event-based sampling method (Miskowicz, 2006).

In this particular case, there will be two error-based logical expressions and two different values of  $\delta$ ,  $\delta = \Delta_P$  for the P part and  $\delta = \Delta_I$  for the I part. The logical expression of each part will depend on the error magnitude that is necessary for the two triggered counterparts to produce the control signal: the error signal for P action and the integrated error (IE) signal for I action.

Once the process is inside the deadband region, defined as  $\alpha y_{sp} < y_{sp} < \beta y_{sp}$ , the set-point following task is over and the disturbance rejection task takes control. Note that the control action is fixed at  $u = u_{ff} = u_{ff}^2 = K_p^{ff} y_{\tau}$ , until a new reference value is introduced. This means that the output of  $C_{ff}$  is constant, and  $C_{fb}$  is enabled and will start computing proportional and integral actions when the process leaves the band as a consequence of a disturbance. We assume that the disturbance  $\omega$  is a piecewise constant signal.

The algorithm of the  $C_{fb}$  controller can be expressed as:

1. 
$$u_{fb} = u_{fb}^{T} = IE = e_{current} = e_{last} = 0$$
;  $y_{ll} = \alpha y_{sp}$ ;  $y_{ul} = \beta y_{sp}$ ;  
2. If  $(y(t) \ge y_{ul})$  then  $e_{current} = y_{ul} - y(t)$   
else if  $(y(t) \le y_{ll})$  then  $e_{current} = y_{ll} - y(t)$ ;  
else  $e_{current} = e_{last} = 0$ ;  
3.  $IE = IE + h_{nom}e_{current}$ ;  
4. If  $(|e_{current} - e_{last}| \ge \Delta_P)$  then  $u_{fb}^{P} = K_{p}e_{current}$ ;  $e_{last} = e_{current}$ ;  
5. If  $(|IE| \ge \Delta_I)$  then  $u_{fb}^{I} = u_{fb}^{I} + (K_{p} / T_{i})IE$ ;  $IE = 0$ ;  
6.  $u_{fb} = u_{fb}^{P} + u_{fb}^{I}$ ;

Note that  $h_{nom}$  corresponds to the sampling period of the sensor, not of the controller. This parameter allows us to simulate the "fast sampling" of the sensor with a digital DAQ. In a real implementation it should be fixed as short as possible to detect accurate crossings.

The main problem with the previous algorithm is the possible unnecessary activation of the controller  $C_{fb}$  during the setpoint following task without disturbances. An alternative solution is to extend the triggering of  $C_{fb}$  always from t = 0when the process output is outside the deadband. One way to do that is to modify the deadband by enclosing the process output trajectory during the set-point following task, that is, from t = 0. The point is to consider a false lower band just to produce the triggering of  $C_{fb}$  while maintaining at the same time the constant original lower limit to calculate the proportional and integral actions.

It is worth studying how to modify the lower band by analysing the impact of the disturbances on the process response. During the transition, positive disturbances push the process output towards the dead band by themselves, so these disturbances are not a problem because they contribute to the earlier activation of the controller  $C_{fb}$ . Thus, the upper limit of the dead band should not be changed. However, negative disturbances avoid the activation of the controller because they make the process output fail to attain the lower limit. The false lower limit should then be designed in such a way that it follows the process response in the absence of negative disturbances. We exploit the FOPDT model to adapt the lower limit. The new false lower limit during the transition will be derived from the step response of the FOPDT model as:

$$y(t) = uK(1 - e^{-((t-L)/T)})$$
(3)

using as input  $u + \alpha y_{sp}/K$ . Therefore, the false deadband is redefined as:

$$\alpha y_{sp} \left( 1 - e^{-((t-L)/T)} \right) \le y_{sp} \le \beta y_{sp} \tag{4}$$

from t = 0. Now, the coupling of the two control tasks is natural because  $C_{fb}$  is always enabled but starts working only when the process output leaves the false deadband because of disturbances. The true deadband

$$\alpha y_{sp} \le y_{sp} \le \beta y_{sp} \tag{5}$$

is used to calculate the error.

### **3. DESCRIBING THE INTERACTIVE TOOL**

This section describes the functionalities of the developed tool, which highlights the concepts described in Section 2. The tool is freely available by contacting the authors and can be used in Windows, Mac, and Linux operating systems without the need for a Sysquake license. One consideration that must be kept in mind is that the tool's main feature interactivity- cannot be easily illustrated with written text. Nonetheless, some of the features and advantages of the application are shown below. The reader is invited to use the tool and personally experience its interactive features.

When developing a tool of this kind, one of the most important things that the developer needs to keep in mind is the organization of the main windows and menus to assist the user in understanding the event-based PI controller described in the previous section. The graphics can be manipulated directly by dragging points, lines, and curves or by using text-edits and sliders. Notice also that for all the graphics available in the tool, the vertical and horizontal scales can be modified using three black triangles available on the graphics ( $\blacktriangle$ ,  $\checkmark$ ). The tool is divided into two main parts, *Model identification screen* and *Control design screen* that can be selected in the upper left hand side using two radio buttons. Each part of the tool is further divided into several sections represented in Figures 3 and 4, which show the two main screens of the interactive tool.

#### 3.1 Model identification screen

The Model Identification screen is shown in Figure 3. This screen is focused on determining the *K*, *T*, and *L* parameters of a first order with a dead time model (FOPDT). The process transfer function to be identified can be modified depending on the option selected from the **Settings** menu. Several examples of transfer function are given, and its parameters can be modified interactively by dragging sliders or setting specific values using text-edits fields. However a free transfer function can be selected (**Interactive TF** option in the **Settings** menu) where the process poles and zeros can be inserted, removed or changed from the **Process Transfer Function** graphic. All these elements are available in the left-hand area of the screen. In the right-hand of the screen, there are different graphical elements.



Fig. 3. Interactive tool user interface for model identification phase

On the top a symbolic representation of the model shows continuously all the changes performed on the model parameters (**Model transfer function**). With this purpose some sliders and text-edits are available in the same area (**Model parameters**). Below these elements, there are two different graphics which represent the input signal (**Input**) and the process step response of the system (**Output**) to be identified in red colour. In the second graph it is also represented the model step response in blue colour. The objective of the model identification is to try that the model step response (blue line) coincides as much as possible with the process step response (red line). The user can try to fit the model in two different ways.

One possibility to modify in an interactive way the model parameters is by using the **Output** graphic. In this sense, it is possible to modify the static model gain using the horizontal dashed blue line in the **Output** graphic. The model time constant and the model delay can also be changed using the vertical blue dashed lines in the **Output** graphic. These options allow the user to find an adequate model for the given process transfer function. A second alternative is using the sliders and text-edits that are available in the Model parameters area. In both cases an optimal model can also be fitted to the given process transfer function using the option called Optimization fitting in the Setting menu. This option uses an optimization algorithm, which tries to obtain the best model for the given data. On the top right corner of the Input graphic the mean square error between the model output and the process output is shown being a reference measurement to obtain the desired model.

# 3.2 Control design screen

The second screen of the tool is shown in Figure 4 and is dedicated to design the event-based PI controller using the FOPDT model obtained in the previous stage.

In the left part of the screen it is now included besides the **Process Parameters** elements the **Event Based PI Controllers Parameters** section. These parameters are the following:  $\lambda$  = speed of the process response,  $\alpha$  ( $\beta$ ) = upper (lower) limit of the deadband region where the integral action of the  $C_{fb}$  controller is enabled,  $K_p$  ( $T_i$ ) = proportional (integral) action of the  $C_{fb}$  controller. Below these elements we include again the **Output** graphic of the *Model identification screen*.

Some guidelines on how to tune the design parameters can be outlined:

- *y<sub>ll</sub>* and *y<sub>ul</sub>* must be defined according to the maximum tolerable steady-state error. The deadband should wrap the noise in a real implementation to avoid trains of events, especially from the P part.
- If  $y_{ll}$  and  $y_{ul}$  are equal to  $y_{sp}$ , the system response oscillates around the set-point value regardless the other parameters.
- Increasing the values of  $\Delta_P$  and  $\Delta_I$  reduces the number of events and the speed and damping of the response.
- A high value of  $\Delta_P$  or  $\Delta_I$  can cancel the P or I part, respectively, as events are not triggered.



Fig. 4. Interactive tool user interface for event based PI controller design phase

- The cancellation of the P part because of a high value of  $\Delta_P$  introduces oscillations in the loop.
- A good compromise between the number of events and the control performance is obtained with  $\Delta_{\rm P}$  and  $\Delta_{\rm I}$ ranging from 2% to 10% of  $y_{sp}$ .

Figure 4 shows an example of the method applied to a second order process P(s) = 2.5/((1+s) (1+0.5s)) with a unit load disturbance step at t = 3.8. The PI parameters  $K_p = 0.95$  and  $T_i = 0.87$  have been determined by applying the well-known SIMC tuning rules (Skogestad, 2003)

### 5. CONCLUSIONS

A new interactive tool for analysis and design of a new 2DOF event based PI controller has been described. The purpose is to enhance the knowledge of these kind of systems by exploiting the advantages of immediately seeing the effects of changes that can never be shown in static pictures. The module has been implemented in Sysquake, a Matlab-like language with fast execution and excellent facilities for interactive graphics.

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